

# But-1-ene isomerization over Nafion<sup>®</sup> resin/silica composite catalyst

Q. Sun, M. A. Harmer and W. E. Farneth

The DuPont Company, Central Research and Development, Experimental Station, PO Box 80356, Wilmington, DE 19880, USA

**But-1-ene isomerization to but-2-enes at 50 °C to near thermodynamic equilibrium is observed over a novel high surface area Nafion<sup>®</sup> resin/silica composite solid acid catalyst at a mass hourly space velocity (MHSV) of but-1-ene of 2.5 h<sup>-1</sup>.**

Traditionally, alkene isomerization and alkylation, important reactions in petroleum refineries, are catalysed by mineral acids like H<sub>2</sub>SO<sub>4</sub>, HF or AlCl<sub>3</sub>. Environmental concerns associated with corrosive mineral-acid catalysts have encouraged process changes and the development of solid-bed catalytic processes. It is very desirable to convert but-1-ene to but-2-enes for the HF catalysed alkylation process because the quality of the alkylates from but-2-enes feed [96–98 research octane number (RON)] is significantly better than that from the but-1-ene (87–89 RON).<sup>1</sup> Various solid-acid catalysts and even amorphous silica-alumina catalyse the but-1-ene isomerization to but-2-enes at near ambient temperatures, but rapid deactivation is frequently encountered.<sup>2–6</sup> Perfluorinated sulfonic acid resin (e.g. Nafion<sup>®</sup> resin), is another possible solid-acid alternative.<sup>7</sup> However, owing to its extremely low surface area (ca. 0.02 m<sup>2</sup> g<sup>-1</sup>),<sup>8</sup> Nafion<sup>®</sup> resin is not an effective catalyst for gas- or liquid-phase reactions where the reactant or solvent could not swell the framework of Nafion<sup>®</sup> resin. Recently, Harmer has developed a highly active high surface area Nafion<sup>®</sup> resin/silica composite material (surface area ≈ 350 m<sup>2</sup> g<sup>-1</sup>)<sup>9</sup> where small Nafion<sup>®</sup> resin particles (<100 nm average diameters) have been entrapped in the porous silica framework during a sol-gel preparation.<sup>10</sup>

In the current study, a 13 mass% Nafion<sup>®</sup> resin/silica composite was used as a catalyst for the but-1-ene isomerization and comparisons were made with pure Nafion<sup>®</sup>-NR50 beads, Amberlyst-15<sup>®</sup> resin, HZSM-5, and amorphous silica-alumina catalysts.

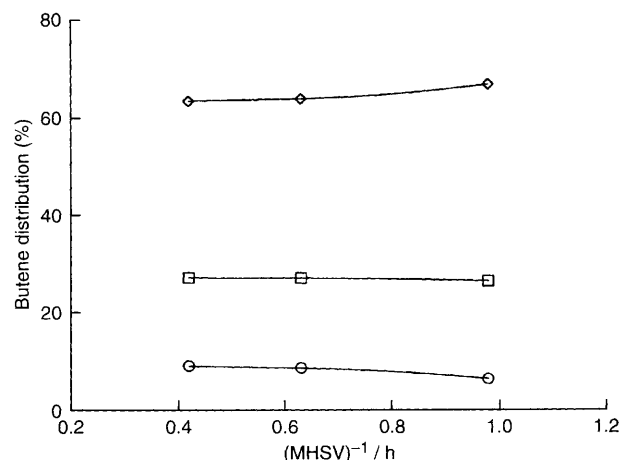
Solid-acid catalysed but-1-ene isomerization to *cis*-but-2-ene, *trans*-but-2-ene and 2-methylpropene was carried out in the temperatures range 23–250 °C and ambient pressure in a 1/2" stainless-steel reactor. Typically, 2.5–5.0 g of catalyst were loaded in the reactor. Prior to the reaction, Nafion<sup>®</sup> resin-based catalysts were dried in a vacuum oven at 150 °C overnight, Amberlyst-15<sup>®</sup> resin was dried at 110 °C overnight, HZSM-5 and silica-alumina were calcined at 400 °C for 2 h. The reactant but-1-ene was diluted with helium. The reaction mixture was analysed by an on-line GC equipped with an FID detector and a 25 m plot column coated with Al<sub>2</sub>O<sub>3</sub>/KCl.

The 13 mass% Nafion<sup>®</sup> resin/silica composite is a very effective catalyst for the but-1-ene to but-2-enes isomerization reaction under mild conditions. Even at 50 °C, near thermodynamic equilibrium values are obtained, which at 50 °C are 4.1, 70.5 and 25.4% for but-1-ene, *trans*-but-2-ene, and *cis*-but-2-ene, respectively,<sup>11</sup> and the experimental data are 6.6, 66.9 and 26.5%, respectively at MHSV of but-1-ene of 1 h<sup>-1</sup> as shown in Fig. 1. The formation of 2-methylpropene and oligomers is negligible below 100 °C. The effective activation energy for but-1-ene isomerization to but-2-enes was determined to be 16.0 kcal mol<sup>-1</sup> (cal = 4.184J) over this 13 mass% Nafion<sup>®</sup> resin/silica composite. Although no catalyst deactivation was observed over more than 12 hours for the but-1-ene isomerization to but-2-enes, at temperatures >100 °C the

formation of 2-methylpropene and oligomers decreased rather rapidly with time on stream.

On the other hand, over the Nafion<sup>®</sup>-NR50 beads but-1-ene conversion was <1% at 50 °C (Table 1). But-1-ene conversion increased gradually with increased reaction temperature up to 200 °C. At the temperature where Nafion<sup>®</sup> resin effectively catalyses the but-1-ene isomerization, ca. 200 °C, significant yields of oligomers of butene (C<sub>8</sub><sup>+</sup> hydrocarbons) and the cracking products of oligomers (C<sub>1</sub>–C<sub>7</sub> hydrocarbons) were also formed. In all cases, 2-methylpropene formation was negligible. A significantly greater amount of oligomers formed over the gel-type Nafion<sup>®</sup>-NR50 beads relative to the composite catalyst under the same reaction conditions.

The commercial macroporous Amberlyst-15<sup>®</sup> resin catalyst (surface area ≈ 45 m<sup>2</sup> g<sup>-1</sup>) on heating to 100 °C is a quite effective catalyst for the but-1-ene isomerization to the linear but-2-enes. At the conditions employed, He:but-1-ene = 1.2:1.0 and MHSV of but-1-ene = 2.5 h<sup>-1</sup>, a near equilibrium *n*-butene distribution, 8.2, 62.8 and 28.8% for but-1-ene, *trans*-but-2-ene and *cis*-but-2-ene, respectively, was obtained at 100 °C. However, at 50 °C only 31.2% of but-1-ene was converted into but-2-enes. Table 2 compares the catalytic



**Fig. 1** Effect of contact time on but-1-ene isomerization over 13 mass% Nafion<sup>®</sup> resin/silica composite catalyst at 50 °C and He:but-1-ene = 1.2:1.0; but-1-ene (○), *cis*-but-2-ene (□), *trans*-but-2-ene (◇)

**Table 1** Product distribution (%) for the but-1-ene isomerization over 5.0 g Nafion<sup>®</sup>-NR50 resin catalyst under ambient pressure with flow rates of He = but-1-ene = 38 ml min<sup>-1</sup>, MHSV of but-1-ene = 1 h<sup>-1</sup>

Butene	T/°C				
	50	100	150	200	250
But-1-ene	>99.0	86.1	38.1	18.6	24.1
<i>trans</i> -But-2-ene	—	5.8	36.0	48.1	42.9
<i>cis</i> -But-2-ene	<1.0	8.0	25.7	31.6	31.0
2-Methylpropene	—	0.1	0.2	1.7	3.0
% Oligomers <sup>a</sup>	—	—	ca. 9	ca. 27	ca. 36

<sup>a</sup> Balanced by butenes.

performances of the above three catalysts at 50 °C and same MHSV of but-1-ene. Even though the 13 mass% Nafion® resin/silica composite has a very low acid capacity, 0.12 mequiv. g<sup>-1</sup> in comparison to the 0.89 mequiv. g<sup>-1</sup> of Nafion®-NR50 resin and 4.6 mequiv g<sup>-1</sup> of the Amberlyst-15® resin, it is still a significantly more active catalyst even based on the unit masses.

Although the initial isomerization activity of the HZSM-5 is very high, extremely rapid loss of catalytic activity was observed. At 23 °C and MHSV of but-1-ene of 2.5 h<sup>-1</sup>, but-1-ene conversion decreased from 48% after 5 min on stream to 5% after 20 min on stream. After being on stream for 30 min at 23 °C, the deactivated catalyst still showed very low activity even at 100 °C, 32% but-1-ene conversion at MHSV = 2.5 h<sup>-1</sup>. Amorphous silica-alumina shows very low initial activity. No but-1-ene conversion can be realized at 50 °C and but-1-ene MHSV of 2.5 h<sup>-1</sup>. Even at 100 °C, but-1-ene conversion is only ca. 6%.

**Table 2** Product distributions (%) for the but-1-ene isomerization over solid-acid catalysts under ambient pressure at 50 °C with He: but-1-ene = 1.2:1.0 and MHSV of but-1-ene = 2.5 h<sup>-1</sup>

Butene	Catalyst		
	Nafion® resin	Amberlyst-15®	13 mass % composite
But-1-ene	> 99.0	69.8	9.2
<i>trans</i> -But-2-ene	—	17.1	63.6
<i>cis</i> -But-2-ene	< 1.0	13.1	27.2

Overall, the extremely low surface area of Nafion®-NR50 beads results in low activity for the but-1-ene isomerization under the reaction conditions employed. However, the intrinsic isomerization activity of the active sites in Nafion® resin is high and when present in a more accessible microstructure it becomes a very effective catalyst. Very high catalytic activity was observed for the 13 mass% Nafion® resin/silica composite material. Equilibrium distribution of *n*-butenes can be readily obtained at 50 °C.

## References

- 1 L. F. Albright, *Oil & Gas Journal*, 1990, Nov. 26th, 70.
- 2 W. O. Haag and H. Pines, *J. Am. Chem. Soc.*, 1960, **82**, 2488.
- 3 A. Ozaki and K. Kimura, *J. Catal.*, 1964, **3**, 395.
- 4 J. W. Hightower, H. R. Gerberich and W. K. Hall, *J. Catal.*, 1967, **7**, 57.
- 5 H. Pines, *The Chemistry of Catalytic Hydrocarbon Conversions*, Academic Press, New York, 1981, ch. 1.
- 6 S. Natarajan, P. A. Wright and J. M. Thomas, *J. Chem. Soc., Chem. Commun.*, 1993, 1861.
- 7 G. A. Olah, P. S. Iyer and G. K. S. Prakash, *Synthesis*, 1986, 513.
- 8 F. J. Waller and R. W. Van Scoyoc, *Chemtech*, 1987, **17**, 438.
- 9 M. A. Harmer, International Publication Number WO95/19222. This patent application describes the preparation of the 13 mass% Nafion® resin/silica nanocomposite. These composites are made via the hydrolysis and condensation of tetramethoxysilane in the presence of a Nafion® resin (Aldrich), in an alcohol-water mixture.
- 10 M. A. Harmer, W. E. Farneth and Q. Sun, *J. Am. Chem. Soc.*, submitted.
- 11 R. H. Perry, D. W. Green and J. O. Maloney, *Perry's Chemical Engineers' Handbook*, 6th edn., McGraw-Hill, New York, 1984, pp. 3–148.

Received, 4th March 1996; Com. 6/01494A